Preparation of dip-coated TiO₂ photocatalyst on ceramic foam pellets

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In recent decades, the photocatalytic reaction has attracted a great deal of attention for the purification of aquatic or atmospheric environments [\[1,](#page-3-0) [2\]](#page-3-1). Especially, titanium dioxide (TiO_2) has been widely utilized as a photocatalyst for generating electrons (e[−]) and holes $(h⁺)$, thereby inducing reductive and oxidative reactions, respectively. The electrons and holes can be excited through UV light irradiation to overcome the band gap energy. Accordingly, O_2^- and OH · radical ions are produced and mineralize pollutants into $CO₂$ and $H₂O$. The highly oxidative ability of photocatalysis is very effective in the detoxication of volatile organic carbon (VOC) pollutants such as phenol. In this case, VOC passes through various reaction steps. The photooxidative reaction mechanisms and the mineralization pathway for the photoreaction of phenol are described schematically in Fig. [1.](#page-0-0)

For deriving an effective photocatalytic reaction, suspended $TiO₂$ particles have been conventionally used. However, there are significant problems such as particle handling and solid/ liquid separation, so $TiO₂$ materials coated on solid supports have been actively studied to overcome these disadvantages. This study proposes a unique and economical coating technique: the dip coating of micro-dimensional $TiO₂$ particles onto ceramic foam pellets with a thickness of several millimeters. The ceramic foams also feature a high porosity (about 80%) but a large pore size (about 100 μ m), and so facilitate the dip-coating with $TiO₂$ particles to produce a photocatalytic reaction with a high efficiency at low cost. In the final section of this letter, we report an experiment on the photodegradation of phenol using prepared pellets with dip-coated $TiO₂$.

The pellets support materials to be coated, were prepared by the following three major processes: slurry preparing, foaming, and pelletizing. These processes have been reported in earlier literature [\[4,](#page-3-2) [5\]](#page-3-3). The raw material for the ceramic foam pellets was silica powder of about 3 μ m in particle size. The pellets undergoing the final pelletizing process were sifted for constant size in the range 3 to 5 mm, and for close to spherical shape. The porosity estimated from bulk, squareshaped, ceramic foams was measured to be about 77%;

Figure 1 A schematic diagram of mechanisms for the photocatalysis (a) and the photocatalytic mineralization (b) of phenol.

the specific surface area using BET (NOVA 1000, Quantachrome, USA) was about 2.04 m^2/g ; and the mean pore diameter using scanning electron microscope (SEM) photographs (JSM-6300, JEOL, Japan) system was about 107 μ m.

After preparation of the supporting pellets, $TiO₂$ particles were coated according to the principle of thermodynamic spontaneous attachment onto the pellet surfaces. The coating suspension consisted of distilled water, polymer dispersant (Darvan 7, R.T. Vanderbilt, USA), and TiO₂ powder of 1.05 μ m in average particle size, which was measured using a particle sizer (Sald 2001, Shimadzu, Japan). A surface electrical property assessed by the zeta potential meter (Zetasizer 2000, Malvern, USA) showed that there might be favorable attachment between them, due to their different kinds of surface charges around pH 5 (Fig. [2\)](#page-1-0).

Figure 2 ζ-potentials of a pellet and TiO₂ according to pH.

In spite of the spontaneous attachment, the coating of $TiO₂$ suspension may be hindered by its high viscosity at a high concentration of the particles in the suspension. Thus, particle concentration and the corresponding viscosity of the suspension were checked using a spectrometer (Hach 2010, Hach, USA) and viscometer (UV II+, Brookfield, USA).

As a result, concentrations less than 5 wt.% or greater than 15 wt.% were found to be inappropriate to form enough coating layers on the pellets, because of insufficient attachment capacity and excess viscosity, respectively. The optimal concentration was determined to be 10 wt.% for a sound coating, and the optimal concentration of dispersant was similarly determined to be 5 wt.%. For an even spread of coating slurry throughout the pellet pores, pressure in the pores was lowered to 0.3 atm for 2 h.

A chemical analysis using ICP (Optima 3000 DV, Perkin Elmer) revealed that the volume of coated $TiO₂$ particles on a pellet occupied as much as 10 wt.% of the whole volume of the pellet. This suggests that the coating suspension was uniformly filled throughout all pores, when it is considering that the slurry penetrating pores contain only 10 wt.% $TiO₂$ in the slurry. SEM photographs of an uncoated pellet and one coated with $TiO₂$ particles are compared in Figs [3](#page-2-0) and [4,](#page-2-1) respectively.

In addition, it is necessary to examine the change of the crystal structures according to calcinating temperature $[1, 2]$ $[1, 2]$ $[1, 2]$. TiO₂ contains small band gap energies, 3.2 eV for anatase phase and 3.0 eV for rutile phase. Even the higher energy, anatase phase, shows a higher photocatalytic efficiency than the rutile because anatase is constructed of a highly activated structure. The ratio between the amounts of phases present in the coated $TiO₂$ can be estimated by the peak ratio produced from an X-ray diffractometer (XRD, DMAX III, Rigaku, Japan), according to the following mathematical formula for the peak ratio (*f*):

$$
f = \frac{1}{1 + 1.26 \frac{I_A}{I_R}}
$$
 (1)

where f is weight fraction of the anatase present, and I_A and I_R are the intensities of primary peaks for anatase and rutile, respectively. Table I shows calculated *f* values for coated and uncoated $TiO₂$, and the specific surface area of coated $TiO₂$, according to heating temperature. Under normal conditions, the anatase phase is converted into rutile phase at 800 ◦C. For the Ti-O-Si bonding of this study, a temperature of $1000 °C$ is required for the corresponding transition [\[2\]](#page-3-1). The *f* values of coated $TiO₂$ with heating temperatures of 500 and 600 ◦C are relatively low because of insufficiently developed crystallization. The values of the specific surface area of coated $TiO₂$ show that the number of

TABLE I *f* values calculated by Equation 1, and specific surface area of TiO₂-coated pellets

Heating temperature $(^{\circ}C)$	$TiO2$ powders	$TiO2$ coated layer	Specific surface $area(m^2/g)$
500	78	64	6.2
600	70	69	6.5
700	46	75	4.2
800	0	30	4.9
1000	0	0	1.4
1200	0	0	1.3

Figure 3 Appearance (a) and cross-sectional area (b) of ceramic foam pellets.

Figure 4 SEM photographs of TiO₂ coated on ceramic foam pellet.

reactive sites decreases as the conversion from anatase to rutile progresses.

Finally, to estimate the photocatalytic effectiveness of the prepared, dip-coated $TiO₂$ particles, the experimental reactions with phenol degradation were executed with shaking for homogenization during the reaction. The phenol of 99.9% purity used in the experiment is a commercial product (Kumho P& B, Korea). A UV light source $(G_{20}T_{10}$, Sanky Denki, Japan) can radiate photoenergy of 68.7 μ W/cm² at 1 m distance with a wavelength of 250 nm. The concentration of phenol was measured by using the spectrometer, after the distillation preprocessing using a Liebig's condenser.

Fig. [5](#page-2-2) presents the first-order photo-degradation of phenol as a function of irradiation time, with variations of heat temperature. The kinetic expression of phenol removal is described as follows:

$$
C = C_0 \exp(-kt) \tag{2}
$$

where C is the concentration of phenol in a reactor; C_0 is the initial concentration of phenol; *k* is the photocatalytic reaction constant; and *t* [s] is the reaction time. $k \, [s^{-1}]$ values obtained by fitting experimental

Figure 5 Photo-degradation of phenol according to the irradiation time in the presence of TiO₂-coated pellets.

data were 1.76×10^{-2} , 2.92×10^{-2} , 2.63×10^{-2} , 1.18 \times 10⁻², 0.49 \times 10⁻², and 0.29 \times 10⁻² s⁻¹, for TiO₂ photocatalyst with heating temperatures of 500, 600,

Figure 6 Variation of turbidities according to shaking time for TiO₂coated pellets.

700, 800, 1000, and 1200 ◦C, respectively. It should be noted that the variation of *k* values is in accordance with that of the specific surface area of coated $TiO₂$; refer to Table I. For evaluating coating adhesion of $TiO₂$ powders on the pellet surface, 5 g of coated pellets were agitated at 120 rpm in 100 cm^3 water using the rotation of a shaker (Jeio Tech, Korea). In the case of the reaction with TiO₂ at 500 and 600 \degree C heating temperatures, many particles were detached from the surface of the pellets and the water turbidity increased, due to a lack of heat treatment of the coating (Fig. [6\)](#page-3-4). When compared with the effectiveness of the uncoated $TiO₂$ particles (1 μ m in size) whose *k* values ranged from 0.55×10^{-2} s⁻¹ to 2.33 × 10⁻² s⁻¹, the dip-coated TiO2 photocatalyst with heating temperatures of 600 and 700 ◦C showed a higher efficiency in photodegradation of phenol. On the other hand, heat treatment at temperatures greater than 800 ◦C was inefficient for phenol removal because of the decrease in specific surface area due to phase-transformation from anatase to rutile phase.

In conclusion, the dip-coating described in this study is advantageous because of its inexpensiveness and the ease of handling of the coating materials. However, there is such a shortage that the reticulate pore structure of the ceramic foam pellets may consume an excessive amount of $TiO₂$ for coating, because coated $TiO₂$ on the inner pore surface may not have photocatalytic activation. Nevertheless, the dip-coated $TiO₂$ showed a better phenol removal effect than the uncoated, at heating temperatures of about 700 ◦C.

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